



## MHD CASSON NANOFLUID FLOW WITH VISCOUS DISSIPATION, CHEMICAL REACTION AND THERMAL RADIATION SUBJECTED TO CONVECTIVE BOUNDARY CONDITIONS

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**ABSTRACT.** Casson nanofluid flow in the presence of nanoparticles, viscous dissipation, chemical reactions and thermal radiations under the influence of convective boundary conditions is numerically investigated. Convective conditions of temperature and nanoparticle concentration are employed in the formulation of the problem. The highly governing partial differential equations models the problem are reduced to ordinary differential equations via similarity variables. Numerical solutions via shooting method with six order Runge Kutta scheme used to solve the velocity, temperature and nanoparticle concentration models. The numerical simulation is carried out with the aid of Maple software. The results and influence of embedded flow parameters are presented through graphs and tables. The obtained results are compared with similar existing results in literature and there is excellent agreement. We found that temperature and nanoparticle concentration fields decrease when the values of Casson parameter increases. It is found that the temperature and concentrations fields enhanced as Biots numbers increases due to thermal and concentration convective conditions. The results further revealed that both the thermal and nanoparticle concentration boundary layer thicknesses are higher for the larger values of thermophoresis parameter. It is also observed that temperature and concentrations profiles reduces for large value of Brownian motion parameters. The results further reveal that both the fluid temperature and concentration increases as chemical reaction increases.

### 1. INTRODUCTION

Nanomaterials are introduced as new energy materials because these materials have particles with size as the same as or smaller than the size of de Broglie

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2010 *Mathematics Subject Classification.* Primary: 22E30. Secondary: 58J05.

*Key words and phrases.* Magenetohydrodyamics nanoparticles; Casson fluid; thermal radiations; thermal and concentration convective conditions; chemical reaction.

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Submitted: September 23, 2024. Revised: October 23, 2024. Accepted: November 5, 2024.

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wave, Hussain et al. (2015) and Sharma et al. (2009). The use of nanoparticles is now a subject of abundant studies. It is due to their Brownian motion and thermophoresis properties. A new class of heat transfer fluids is known as nanofluids (a base fluid and nanoparticles). The nanoparticles are utilized to enhance the heat transfer performance of the base fluids, Choi and Eastman (1995). The cooling rate requirements cannot be obtained by the ordinary heat transfer fluids because their thermal conductivity is not adequate. Brownian motion of the nanoparticles enhance the thermal conductivity of base fluids. Further, the magnetic nanofluid is a unique material that has properties of both liquid and magnet. The magnetonano-fluid is important for cancer therapy, construction of loud speakers, blood analysis, and etc. Many of physical characteristics of nanofluids can be controlled and adjusted by varying an applied magnetic field. Hosseini and Ghader (2010) provided a model to analyze the viscosity of nanofluid with temperature and particle volume fraction. Kandasamy et al (2011) investigated the MHD boundary layer flow over a vertical stretching surface in the presence of nanoparticles. They also consider the Suction/blowing effects of their work. They obtained the exact solutions for translational symmetry and numerical solutions for scaling symmetry. Mixed convection flow of nanofluid with magnetic field, suction/injection, viscous dissipation and chemical reaction effects were numerically investigated by Kameswaran et al (2012). Turkyilmazoglu (2012) provided closed form solutions for hydromagnetic thermal slip flow of nanofluid over a linearly stretched surface. Entropy generation analysis in MHD flow of nanofluid was discussed by Rashidi et al (2013). Here, the flow generation is due to the rotation of porous disk. They provided numerical solutions by employing RungeKutta fourth order procedure. Forced convection flow of nanofluid over a horizontal plate was examined by Hatami et al. (2013). Makinde et al. (2013) discussed the buoyancy-driven stagnation point flow of nanofluid over a convectively heated stretching and shrinking surfaces. Hatami and Ganji (2013) investigated the effect of heat transfer in non-Newtonian nanofluid passing through a porous medium. Hussain et al. (2015) investigated the flow of Casson nanofluid with viscous dissipation and convective conditions: A mathematical model. They implored homotopy perturbation analysis (HAM) as method of solution. Boundary layer flows with combined heat and mass transfer over a stretching or moving surfaces are quite essential in many industrial and metallurgical processes. Such situations occur in the design of chemical processing, damage of crops due to freezing, cooling of drying and papers in textile, food processing, cooling towers refrigeration and air conditioning, compact heat exchangers, solar power collectors, cooling of an infinite metallic plate in a cooling bath etc. Various researchers analyzed such flow analysis for different fluid models under isothermal heat and mass conditions, Motsa et al. (2011), Mahmood et al (2013), Turkyilmazoglu (2013), Alsaadi et al (2013), Ferdows et al. (2013). The concept of convective heat condition is quite popular amongst the researchers. Aziz () carried out an analysis to discuss the steady laminar flow over a flat plate with convective boundary condition. Makinde and Aziz (2010) extended the work of Aziz (2009) by considering the MHD flow through a porous medium

with buoyancy force. Makinde and Aziz (2010) also analyzed the variable diffusivity fluid combined with heat and mass transfer in the presence of thermal boundary condition. Three-dimensional boundary layer flow of Jeffery fluid with convective surface condition was discussed by Shehzad et al (2014). Hayat et al. (2013) presented homotopic solutions of buoyancy driven flow of Maxwell fluid near a stagnation point in the presence of convective condition. Boundary layer flow of nanofluid with thermal convective boundary condition was investigated by Makinde and Aziz(2011). Alsaedi et al. (2012) extended the analysis of Makinde and Aziz (2011) by considering stagnation point flow with heat generation/absorption. The present investigation is focused on MHD casson nanofluid flow in the presence of chemical reaction, thermal radiation and viscous dissipation. The problem is subjected to thermal and convective boundary conditions. Further, the Partial differential equation models governing the models are reduced to Ordinary differential equation via similarity variable and the reduced system of equations are solve by shooting method and six order Rung Kutta method. Simulation of the code is carried out using Maple. Graphs and Tables are used to present the numerical results. There is excellent agreement between the obtained results and the similar existing results in literature when compared. We also extend the work of Shahmohamadi (2012), Hayat et al. (2012), Mukhopadhyay (2013), Hussain et al. (2015) to magneto hydrodynamic (MHD) boundary layer flow of Casson nanofluid over an exponentially stretching surface.

## 2. PROBLEM DEVELOPMENT

We examine magneto hydrodynamic (MHD) flow of Casson nanofluid over an exponentially stretching sheet in the presence of chemical reactions, thermal radiation and viscouse dissipations. The fluid is taken to be incompressible. We assume that the surface of sheet is heated by a hot fluid with temperature and concentration that give heat and mass transfer coefficients and . Magnetic field of strength is applied normally to the flow. The magnetic Reynolds number is chosen to be small. The induced magnetic field is smaller in comparison with the applied magnetic field and thus neglected. Following Makinde and Aziz (2011), Alsaedi (2012), Shahmohamadi (2012) and Hussain et al. (2015), the MHD boundary layer equations of Casson nanofluid are

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{2.1}$$

$$u \frac{\partial T}{\partial x} + \frac{\partial v}{\partial y} = \left(1 + \frac{1}{\beta}\right) \frac{\partial^2 u}{\partial y^2} - \frac{\sigma \beta_0^2}{\rho_f} u \tag{2.2}$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} + r \left( D_B \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} + \frac{D_r}{T_\infty} \left( \frac{\partial T}{\partial y} \right)^2 \right) + \frac{v}{c_p} \left( 1 + \frac{1}{\beta} \right) \left( \frac{\partial u}{\partial y} \right)^2 - \frac{1}{(\rho C)_f} - \frac{\partial q_r}{\partial y} \tag{2.3}$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = \left( D_B \frac{\partial^2 C}{\partial y^2} \right) + \frac{D_r}{T_\infty} \frac{\partial^2 T}{\partial y} - K(C - C_\infty) \quad (2.4)$$

The boundary conditions for the considered flow analysis are

$$\begin{aligned} u = u_w(x) = U_0 \exp(\text{frac}xL), v = 0, -k \frac{\partial T}{\partial y} = h_1 (T_f - T), \\ -D_B \frac{\partial C}{\partial y} = h_2 (C_f - C), \text{ at } y = 0; \\ u \rightarrow, v \rightarrow, T \rightarrow T_\infty, C \rightarrow C_\infty, \text{ when } y \rightarrow \infty. \end{aligned} \quad (2.5)$$

Where  $u$  and  $v$  are the velocity components in the  $x$  and  $y$  direction;  $\nu$  is the kinematic viscosity;  $\beta$  is the Casson parameter;  $\rho$  is the density of fluid;  $\sigma$  is the Stefan-Boltzmann constant;  $\alpha$  is the thermal diffusivity;  $r = \frac{(\rho c)_p}{(\rho c)_f}$  is the ratio of nanoparticle heat capacity and the base fluid heat capacity;  $\nu$  is the kinematic viscosity;  $c_p$  is the specific heat capacity;  $D_B$  is the Brownian diffusion coefficient;  $D_T$  is the thermophoretic diffusion coefficient;  $k$  is the thermal conductivity;  $h_1$  and  $h_2$  are the heat and mass transfer coefficients, respectively;  $T_\infty$  and  $C_\infty$  are the ambient fluid temperature and concentration, respectively,  $K$  is the constant rate of chemical reactions,  $q$  is the radiative heat flux PDE Equations (2.2)-(2.5) is reduced into the dimensionless ODE form by introducing the following new variables:

$$\begin{aligned} \eta = y \sqrt{\frac{U_0}{2\nu L}} \exp\left(\frac{x}{2L}\right), u = U_0 \exp\left(\frac{x}{L}\right) f'(\eta) \\ v = -\sqrt{\frac{\nu U_0}{2L}} \exp\left(\frac{x}{2L}\right), (f'(\eta) + \eta f''(\eta)) \\ A \exp\left(\frac{ax}{2L}\right) \theta(\eta) = \frac{T - T_\infty}{T_f - T_\infty}, B \exp\left(\frac{ax}{2L}\right) \phi(\eta) = \frac{C - C_\infty}{C_f - C_\infty}, \end{aligned} \quad (2.6)$$

The equations of linear momentum, energy and concentration in dimensionless form become

$$\left(1 + \frac{1}{\beta}\right) f'' + f'' - 2f'^2 - M^2 f' = 0 \quad (2.7)$$

$$\theta' + Pr f \theta' + Pr Nb \theta' \phi' + Pr Nt \theta'^2 + Pr Ec \left(1 + \frac{1}{\beta}\right) f''^2 = 0 \quad (2.8)$$

$$\theta' + Le f \theta' + (N_t IN_b) \theta' = 0 \quad (2.9)$$

$$\begin{aligned} f = 0, f' = 1, \theta' = -Bi_1(1 - \theta(0)), \phi' = -Bi_2(1 - \phi(0)), \\ \text{at } \eta = 0, f' \rightarrow 0, \theta \rightarrow 0, \phi \rightarrow 0, \text{ as } \eta \rightarrow \infty. \end{aligned} \quad (2.10)$$

where  $M^2 = \frac{2\sigma B_0^2 L}{(\rho_f U_0 \exp(x/L))}$  is the magnetic parameter  $Pr = \nu/\alpha$  is the Prandtl number,  $Le = \frac{\nu}{D_B}$  is the Lewis number;  $Nb = \frac{(\rho c)_p D_B (C_f - C_\infty)}{(\rho c)_f \nu}$  is the Brownian motion parameter;  $Nt = \frac{(\rho c)_p D_B (T_f - T_\infty)}{(\rho c)_f \nu T_\infty}$  is the thermophoresis parameter;  $Bi_1 = (h_1/k) \sqrt{\nu/a}$ ,  $Bi_2 = (h_2/D_B) \sqrt{\nu/a}$  are the Biot numbers. Equation (1.1)

is satisfied identically. The skin friction coefficient, the local Nusselt number and the local Sherwood number are

$$C_f = \frac{r_w}{\rho_f u_w^2(x)}, Nu_x = \frac{xq_w}{k(T_f - T_\infty)}, Sh_x = \frac{xq_m}{D_B(C_f - C_\infty)} \quad (2.11)$$

where  $r_w$  is the shear stress along the stretching surface;  $q_w$  is the surface heat flux;  $q_m$  is the surface mass flux. The local skin-friction coefficient, local Nusselt and local Sherwood numbers in dimensionless forms are given below:

$$\sqrt{2Re_x C_{fx}} = \left(1 + \frac{1}{\beta}\right) f'(0), \sqrt{\frac{2L}{x}} Nu_x / Re_x^{1/2} = -\theta'(0), \sqrt{\frac{2L}{x}} Sh_x / Re_x^{1/2} = -\phi'(0) \quad (2.12)$$

where  $Re_x = u_w(x)L/v$  is the local Reynolds number.

### 3. DISCUSSION OF NUMERICAL RESULTS

The system of highly nonlinear differential equations (2.7), (2.8) and (2.9) subjected to boundary conditions (2.10) are solved by a numerical approach via shooting method and six-order Runge-Kutta method for different moderate values of the flow, heat and mass transfer parameters. The effective Broyden technique is adopted in order to improve the initial guesses and to satisfy the boundary conditions at infinity. Maple software is used to code and simulate the above numerical procedure. Analysis of variations of Casson parameter  $\beta$ , magnetic parameter  $M$ , Prandtl number  $Pr$ , Lewis number  $Le$ , Biot number  $Bi_1$ , thermophoretic parameter  $Nt$ , Brownian motion parameter  $Nb$  and Eckert number  $Ec$  on the dimensionless temperature  $\theta(\eta)$  is carried out in figures 18. Figure 1 shows that the temperature and thermal boundary layer thickness decrease for the higher values of Casson parameter. Higher value of Casson parameter corresponds to a decrease in the yield stress that causes a reduction in the fluid temperature and thermal boundary layer thickness. Figure 2 illustrates the effects of magnetic parameter on the temperature. Here, an increase in magnetic parameter leads to an enhancement in the temperature. Physically, larger value of magnetic parameter shows stronger Lorentz force. Such stronger Lorentz force is an agent providing more heat to fluid due to the fact that higher temperature and thicker thermal boundary layer thickness occur. Figure 3 shows that the temperature and thermal boundary layer thickness decrease for higher Prandtl numbers. Prandtl number is the ratio of momentum diffusivity to thermal diffusivity. For higher Prandtl fluids the momentum diffusivity increases while there is decrease in the thermal diffusivity. Here, a decrease in thermal diffusivity dominant is over an increase in the momentum diffusivity. This change in thermal diffusivity shows lower temperature and thinner thermal boundary layer.

TABLE 1. Numerical value of skin-friction coefficient  $\left(1 + \frac{1}{\beta}\right) f'(0)$  for different values of  $\beta$  and  $M$  when compared with Hussain et al. (2015)

		$-\left(1 + \frac{1}{\beta}\right) f'(0)$	$-\left(1 + \frac{1}{\beta}\right) f'(0)$
$\beta$	$M$	Hussain et al.(2015)	Present Result
0.7	0.5	2.146677	2.14667722
1.2		1.865142	1.86514231
1.6		1.755974	1.75597401
2.0		1.687085	1.68708521
1.2	0.0	1.735577	1.73557701
	0.4	1.819679	1.81967911
	0.7	1.980908	1.98090831
	1.2	2.205917	2.20591723

TABLE 2. Comparison of value of  $\theta'(0)$  for different values of  $Pr$  with previous existing result  $Nt = Nb = 0.0, \beta \rightarrow \alpha$  when and  $Bi_1 = 1000$  when compared with Makinde And Aziz (2011), Alsaedi et al. (2012) and Hussain et al. (2015)

	$-\theta'(0)$	$-\theta'(0)$	$-\theta'(0)$	$-\theta'(0)$
$Pr$	Makinde and Aziz (2011)	Alsaedi et al (2012)	Hussain et al (2015)	Present Result
0.07	0.0663	0.0663	0.06637	0.066371
0.20	0.1691	0.1691	0.61913	0.619131
0.70	0.4539	0.4539	0.45395	0.453950
2.00	0.9113	0.9113	0.91132	0.911323

Table 1 presents the numerical value of skin-friction coefficient  $-\left(1 + \frac{1}{\beta}\right) f'(0)$  for various values of  $\beta$  and  $M$ . The values of skin-friction coefficient are decreased by increasing  $\beta$  but it increases for higher values of magnetic parameter  $M$ . Table 3 shows an excellent agreement with the previous numerical when compared with some existing result in literature

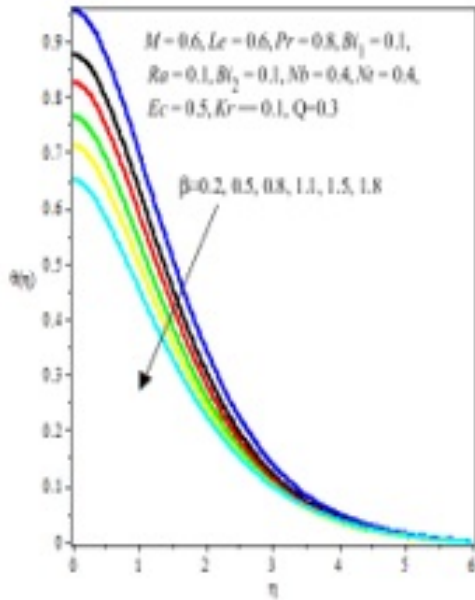


Fig1: Effect of  $\beta$  on Temperature distribution

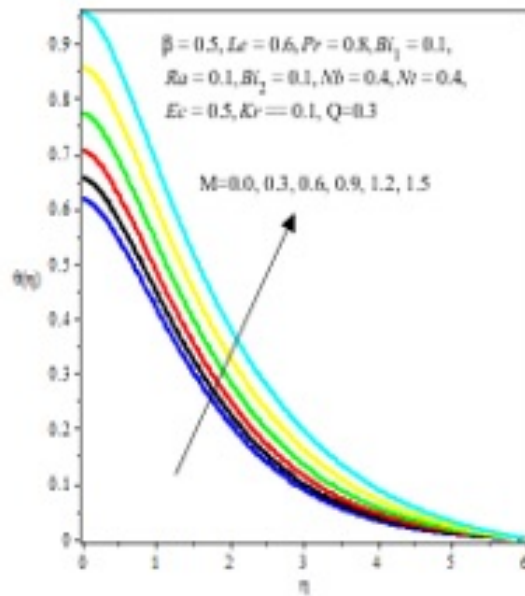


Fig2: Effect of  $M$  on Temperature distribution

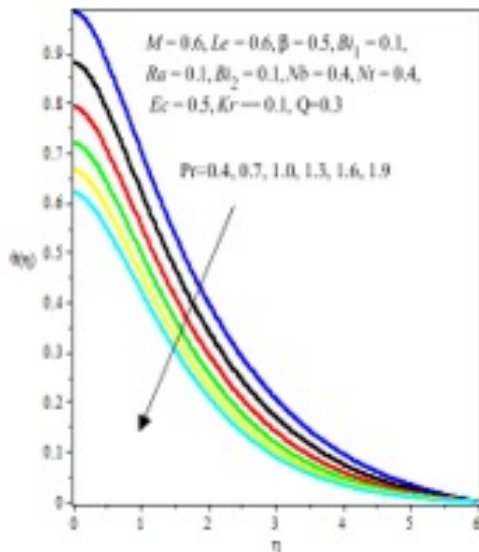


Fig3: Effect of  $Pr$  on Temperature distribution

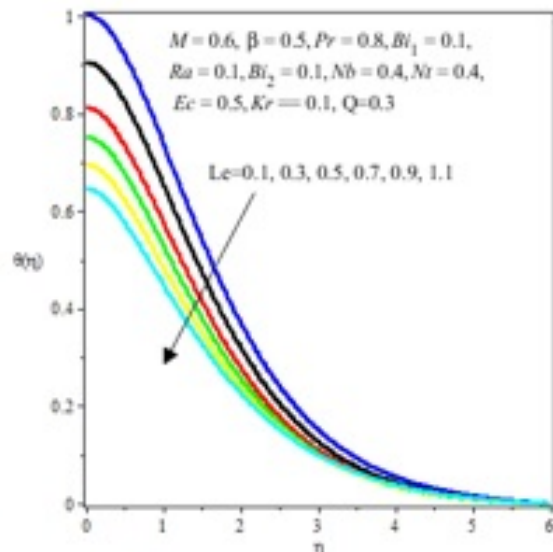
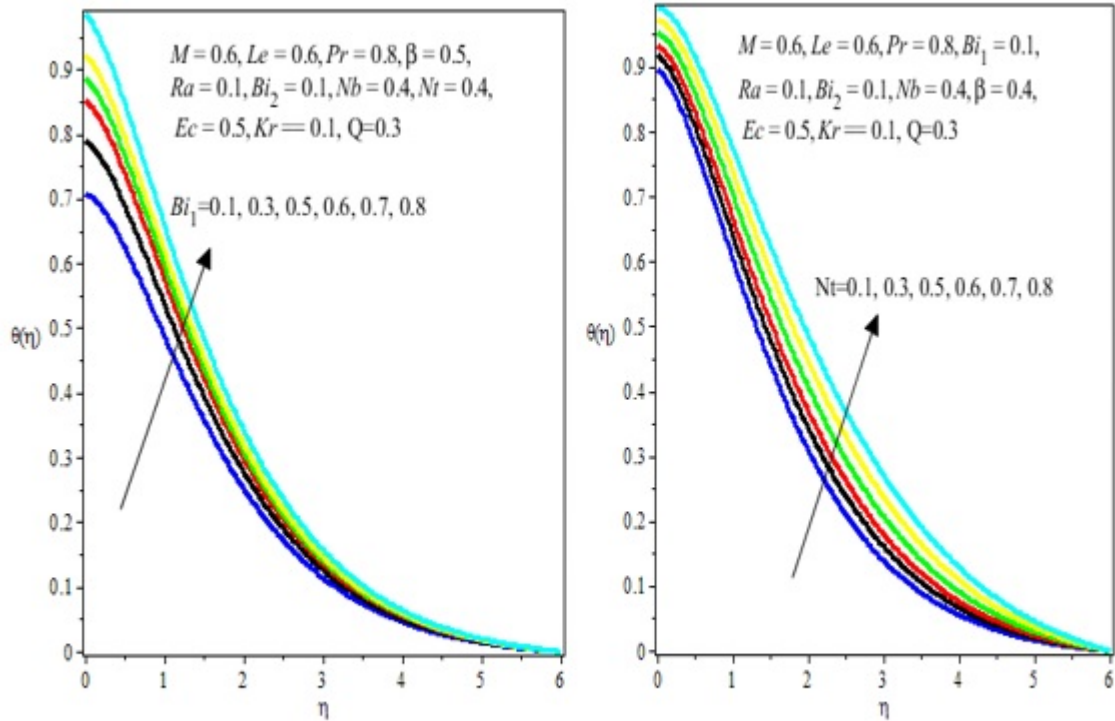


Fig4: Effect of  $Le$  on Temperature distribution

The variations in temperature profile for various values of Lewis number are seen in Fig. 4. Temperature increases for smaller values of Lewis number while it increases for higher values of  $Le$ . It is known that higher Lewis number fluid has smaller Brownian diffusion coefficient and lower Lewis number fluid has higher Brownian diffusion coefficient. This produces a change in temperature and thermal boundary layer



**Fig5: Effect of  $Bi_1$  on Temperature distribution**      **Fig6: Effect of  $Nt$  on Temperature distribution**

Thickness. Figure 5 depicts the change in temperature profile for different values of Biot number  $Bi_1$ . Temperature increases steadily as  $Bi_1$  increases. Figures 6 and 7 elucidate that both temperature and thermal boundary layer thickness increase through larger thermophoretic and Brownian motion parameters. Figure 8 analyzes that temperature is larger for higher values of Eckert number. Figures 9-15 are drawn to examine the change in nanoparticle concentration distribution  $\phi(\eta)$  for different values of Casson parameter  $\beta$ , magnetic parameter  $M$ , Prandtl number  $Pr$ , Lewis number  $Le$ , Biot number  $Bi_2$ , thermophoretic parameter  $Nt$  and Brownian motion parameter  $Nb$ .



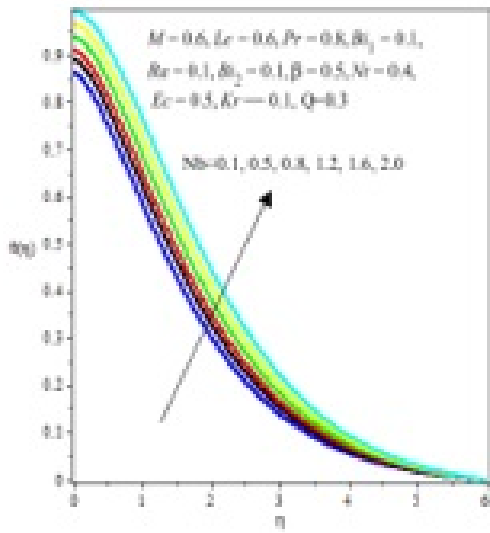


Fig7: Effect of  $Nb$  on Temperature distribution

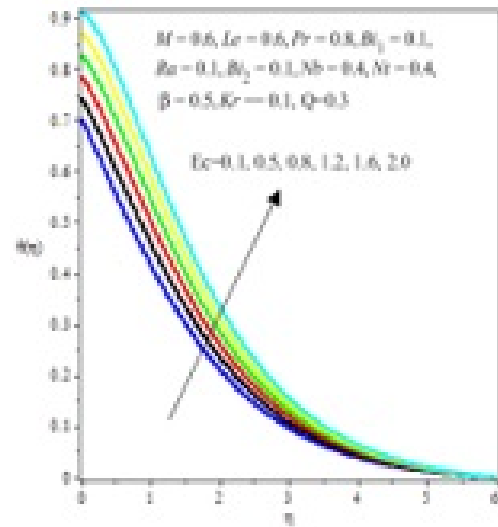


Fig8: Effect of  $Ec$  on Temperature distribution

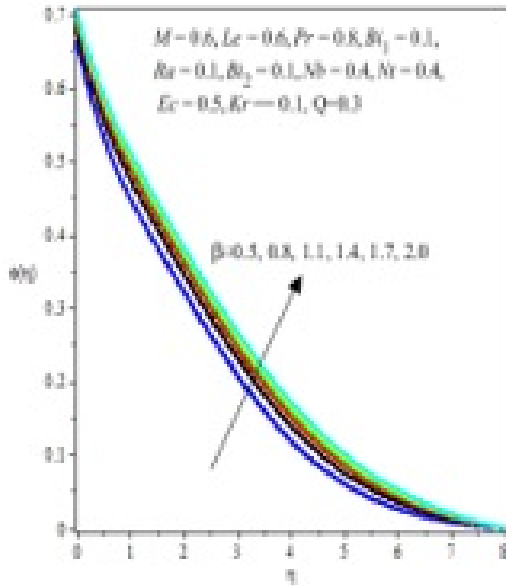


Fig9: Effect of  $\beta$  on concentration distribution

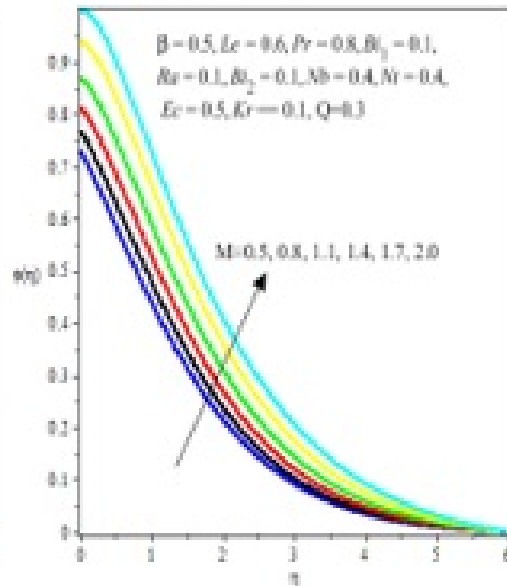
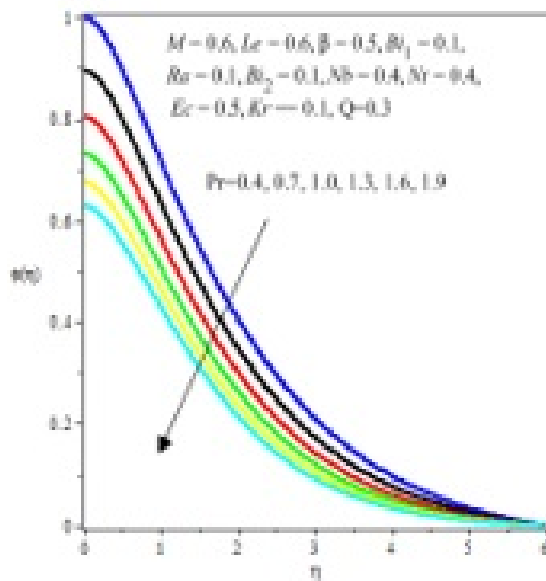
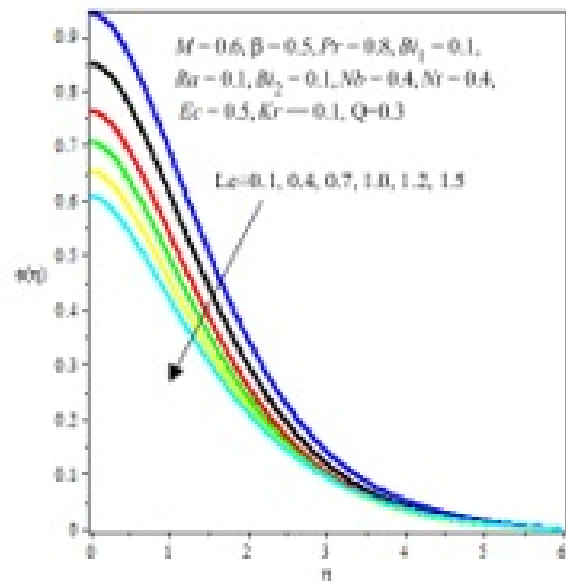
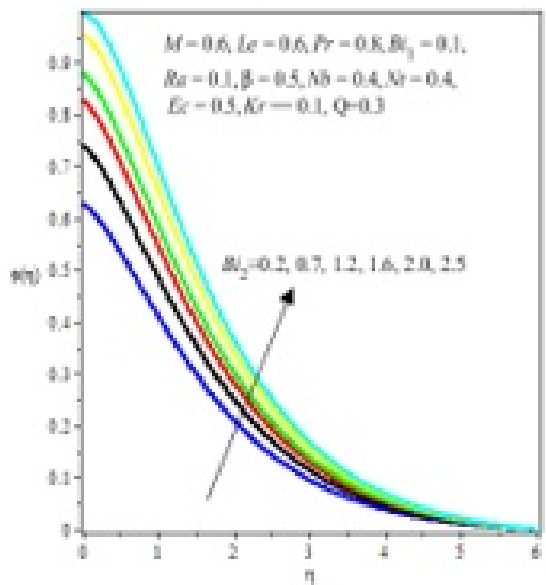
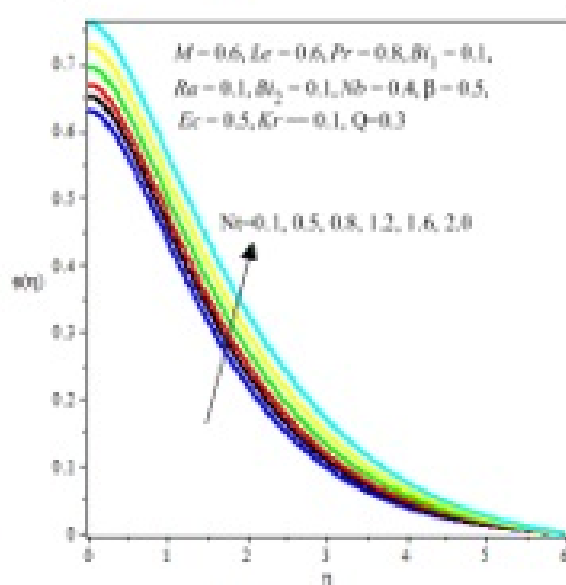


Fig10: Effect of  $M$  on Concentration distribution

Fig11: Effect of  $Pr$  on concentration distributionFig12: Effect of  $Le$  on Concentration distributionFig13: Effect of  $Bi_2$  on concentration distributionFig14: Effect of  $Nr$  on Concentration distribution

Figures 9 and 10 clearly show that Casson and magnetic parameters have similar effects on the nanoparticle concentration and temperature fields. Figures 11 and 12 indicate that the nanoparticle concentration and its related boundary layer thickness decreases when we increase the values of Prandtl and Lewis numbers. An increase in Biot number  $Bi_2$  gives rise to the nanoparticle concentration profile. Nanoparticle concentration profile increases rapidly as  $Bi_2$  increases but this change in nanoparticle concentration is slow down for higher value of  $Bi_2$  and so on (Fig. 13). In fact,  $Bi_2$  involves the Brownian diffusion coefficient. Brownian

diffusion coefficient increases when we increase the values of  $Bi_2$ . This increase in Brownian diffusion coefficient leads to the higher nanoparticle concentration. Figures 14 and 15 show that the nanoparticle concentration is an increasing function of thermophoretic parameter while on the other hand we observed that the nanoparticle concentration decreases when Brownian motion parameter increases. Figure 15 illustrates that the change in nanoparticle concentration corresponding is more dominant for higher value of  $Nb$ . Figure 16 shows the influence of chemical reactions on concentrations profile. Concentration profile increases as chemical reaction increases due to the reaction nano particles in the base fluid

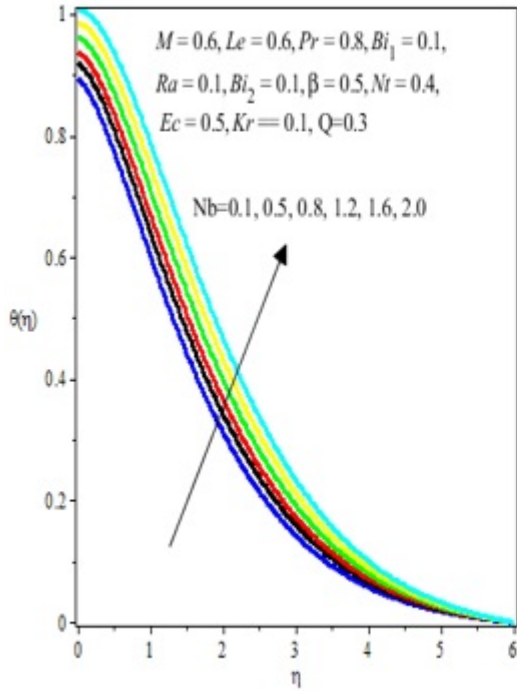


Fig15: Effect of  $Nb$  on concentration distribution

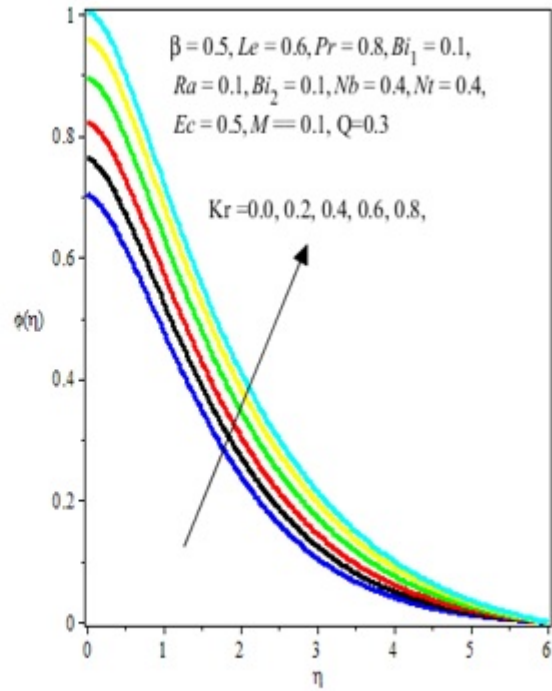


Fig16: Effect of  $Kr$  on concentration distribution

#### 4. CONCLUSIONS

This research paper focuses on analysis of magnetohydrodynamics Casson nanofluid flow with viscous dissipation, thermal radiation and chemical reaction under the influence of convective boundary conditions. The influence of embedded governing flows parameters are analyses and presented graphically and in tabular. The result revealed that higher value of Casson parameter leads to a decrease in the temperature and nanoparticle concentration. Effects of Lewis number on nanoparticle concentration are more pronounced in comparison with the temperature. Increasing values of Biot numbers  $Bi_1$  and  $Bi_2$  correspond to an increase in the fluid temperature and nanoparticle concentration. Temperature is enhanced for the higher values of thermophoresis and Brownian motion parameters. Effects of thermophoresis and Brownian motion parameters on nanoparticle concentration are quite opposite.

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